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(54) **POLYMER EXTRUSION DIE**

EXTRUSIONSDUSE FÜR POLYMERE

FILIERE D'EXTRUSION DE POLYMERES

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• PATENT ABSTRACTS OF JAPAN vol. 10 no. 139
(C-348) ,22 May 1986 & JP,A,61 000614
(KURARAY K.K.) 6 January 1986,

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Description

FIELD OF THE INVENTION

[0001] This invention concerns an improved die for the extrusion of polymers, wherein the exit of the die orifice(s) is flared, and the flared and unflared sections have specified relative dimensions and shapes.

TECHNICAL BACKGROUND

[0002] Extrusion of polymers through a die to form shaped extrudates is a well known process, and is extensively used commercially, see for instance H. Mark, et al., Ed., Encyclopedia of Polymer Science and Engineering, 2nd Ed., vol. 6, John Wiley & Sons, New York, 1986, p. 571-631 and p. 802-824 (fibers), which is hereby included by reference. Items that can be made by polymer extrusion include films, fibers, sheet, strands (including those strands to be cut into pellets for further processing), and shaped profiles. The extrudates are usually essentially continuous, and are often cut into useable lengths.

[0003] The extrusion process is one in which the molten polymer is forced through a shaped orifice, and the extrudate is then cooled, usually until solid. The cross section of the extrudate (perpendicular to the flow direction) usually has the same shape as the orifice. Due to the importance of extrusion commercially, improved dies are constantly being sought, so that the process runs more cheaply, and/or with less off-quality production, etc. A particular problem in this process is "die drips", which are small portions of (usually) molten polymer which collect around the die orifice, and which can cause problems of product defects and downtime.

[0004] U.S. Patent 4,822,546 describes a polymer extrusion die which is advantageous for use with high flow polymers and wherein the die is part of an underwater pelletizer. There is no mention of the use of this die in other extrusion processes.

[0005] European Patent Application 0 566 276 A1 discloses an improved plastics extruder die wherein molten plastic enters the die through an opening of a smaller diameter and exits the die through an extrusion orifice of a larger diameter. In particular, the ratio of the diameter of the extrusion orifice to that of the channel in the die plate through which molten polymer enters the extrusion orifice is 1.1-2.0. The ratio of the diameter to the length of the enlarged portion is 1.06 to 0.6. That die is to enable prevention or substantial reduction of the formation of resin masses in the vicinity of the die phase.

SUMMARY OF THE INVENTION

[0006] The invention as claimed in claim 1 solves the problem of how to prevent small portions of molten polymer collecting around the die orifice.

[0007] The invention is also directed to a polymer

extrusion apparatus comprising such a die and the use of the die for the extrusion of polymer.

DETAILS OF THE INVENTION

[0008] The disclosure concerning the die and its orifices herein applies to the die itself, the die when included in an extrusion apparatus, and the die when used in the process of extruding polymer.

DESCRIPTION OF THE DRAWINGS

[0009] The Figures herein are not to scale.

[0010] A cross section of a flared die orifice, with one step in Z_2 (see below), of this invention is shown in Figure 1. This cross section is perpendicular to surface S_5 (see below). Only a part of the die body having one orifice is shown. The die may contain more than one orifice, and also may have other functional parts that extrusion dies may normally have, such as a means for attached the die to the extrusion apparatus, a means for measuring the temperature of the die, a means for heating the die, a means for sealing the contact surfaces between the die and the remainder of the extrusion apparatus (so molten polymer will not leak), etc.

[0011] Through the length of the orifice, the orifice can be considered to have three zones, a first zone Z_1 having surface S_1 , a third (flared) zone Z_3 having surface S_3 , and a second or transition zone Z_2 having surface S_2 . S_4 of Figure 1 is the surface on the inlet side of the die, while S_5 is the surface on the outlet or discharge side of the die. S_4 need not be flat, and S_5 must be flat and perpendicular to A only in proximity to the orifice (close enough for extrudate to touch S_5). It is preferred if S_1 is approximately parallel to polymer flow axis A (by approximately parallel is meant plus or minus 5°), and more preferred if it is S_1 is parallel to A. S_3 , the orifice surface of Z_3 , is parallel to the polymer flow axis A and perpendicular to surface S_5 .

[0012] Cross sections AA and BB of the die in Figure 1 are perpendicular to flow axis A. L_1 is the total length of the orifice, while L_3 is the length of zone Z_3 . The cross sections at AA and BB go through the (complete) orifice shown in Figure 1. The cross section BB is taken at a spot near where zones Z_1 and Z_2 meet, but it is in Z_1 . The area of the orifice at the cross section AA is about 1.1 to 1.7 times the area of the same orifice at cross section BB, preferably about 1.3 to 1.45 (or the area after each step in Z_2 is at least 1.1 times the area of Z_1 or the previous step). L_1/L_3 is about two or more, preferably about 2 to about 20, and more preferably about 3 or more or about 3 to about 10.

[0013] The cross sections of the orifice at AA and BB are substantially geometrically similar to each other. By geometrically similar is meant "Two geometric figures are similar if one can be made congruent to the other by using a transformation of similitude, i.e., if one is a magnification or reduction of the other.", definition of "simi-

lar" from James and James Mathematics Dictionary, 3rd Ed., D. Van Nostrand Co., Inc., Princeton, NJ, 1968, p. 331. In other words the orifice cross section at BB is a reduction in size of the cross section at AA, so that the area of the orifice cross section at AA is 1.1 to 1.7 times that at cross section AA.

[0014] The angle T is the angle formed by S_2 and A or approximately at which the orifice transitions from S_1 to S_2 , if Z_2 contains one step. This transition may be in one step or a series of steps. The transition zone step(s) may also be in the form of a curve. The line R is then taken as a tangent to the curve at the point at which the curve meets the surface of Z_1 . In a preferred die, angle T (or angles analogous to T in which Z_2 has more than one step) is about 60° to 90° .

[0015] Figure 2 is an outline of the orifice used in the Examples herein. It is described in those Examples.

[0016] As the polymer flows into Z_1 it of course assumes the cross sectional shape of Z_1 (cross section at BB). As the polymer flows through the transition zone, and then into Z_3 , it expands to have a cross section such as that at AA, i.e., it eventually matches the shape and size of the orifice at Z_3 . The polymer exiting the die will therefore have the shape and approximate size of the cross section at AA if L_3 is long enough (the cross section of the polymer exiting the die may be somewhat larger than the orifice cross section at AA due to the well known phenomenon of "die swell"). While Z_1 is necessary for the die orifice herein, the die may also include an "extension" of Z_1 (but not part of L_1 or Z_1) which is not necessarily the same size and/or shape as Z_1 , which extension conducts melted polymer to Z_1 .

[0017] Within Z_2 , there may be one, or more than one, change in the area of orifice. Each change is herein termed a step. If there is a single step, the only requirement for Z_2 is the angle T be about 45° to 90° . Z_3 , immediately adjacent to the step, has S_3 as its surface. If there is more than one step, each step has an angle which corresponds or is analogous to angle T when there is only one step. Each of these angles must also be about 45° about 90° . Only the orifice surface downstream (as the polymer flows) of the last step is S_3 . All of the other surfaces in Z_2 which correspond to S_3 (herein collectively S_{2A}) in each of the other steps is in Z_2 , and each of these surfaces is parallel to A. It is preferred that each of these surfaces parallel to A are long enough so that before the next step the polymer is substantially in contact with the periphery of each surface S_{2A} .

[0018] It is believed that the minimum value of L_3 is desirable because it allows the polymer to substantially achieve the final shape and size desired for the extrudate. By "substantially in contact with" is meant the polymer is either in contact with, or within 0.13 mm of the surface (S_3 and/or S_{2A}).

[0019] It is believed that S_3 and S_{2A} should not extend too much longer than the length required for the polymer to substantially contact the full periphery of S_3 or

S_{2A} . The length needed (of S_3 or S_{2A}) for any particular process, which includes the variables of extrudate shape and size, polymer used, polymer temperature, extrusion rate, etc., can be readily determined by simple routine experimentation, by varying L_3 in a series of die inserts, as inserts were used in the Examples herein.

[0020] The die may be made out of any material that polymer extrusion dies are usually made out of, such as tool steel. Care should be taken to avoid nicks and other blemishes on the orifice surfaces, especially at angled surfaces. The surface finish of the die should be that normally given to extrusion dies. All measurements herein are construed to have the usual machining and other fabrication errors normal in die manufacture.

[0021] The extrusion die may contain one or more orifices. Many dies have only one orifice, particularly if the cross section of the orifice is large. Other dies such as those for forming fibers (often called spinnerets) usually have many orifices. It is preferred if the cross sections at AA (Z_1) and BB (Z_2) (and hence the orifice) are both circular, both square or rectangular.

[0022] The extrusion may be carried out in any apparatus in which extrusions are normally done. Such an apparatus usually includes a means for melting the polymer (except if molten polymer is supplied to the apparatus), and a means to pump or force the molten polymer through the die orifices at an appropriate rate. Useful devices for pumping or melting and pumping are gear pumps, single and twin screw extruders, pistons (as in a ram extruder), or a pressurized vessel (as by gas pressure) containing molten polymer. Extrusion conditions, such as polymer temperature, may be those normally used in extrusions of that polymer.

[0023] After exiting the extrusion die the polymer is usually solidified (or in the case of elastomers may be crosslinked). Thermoplastics are normally solidified by cooling. The cooling medium may be air or a liquid such as water. If the cooling medium is a liquid, the liquid is not in contact with surface S_5 of the die. If the extrudate is to be cut into pieces, such as pellets, it is preferred if the cutter (blade) is not in direct contact with the die, particularly surface S_5 .

[0024] The polymers useful with the extrusion die described herein include thermoplastics, elastomers before crosslinking, and thermosets before crosslinking. Thermoplastics include polyesters, polyamides, polyethers, polyolefins, halogenated polyolefins, fluorinated polyolefins, thermoplastic polyimides, poly(imide-ethers) and polycarbonates, and the like. Polymers which are extruded may contain the usual additives such as fillers, reinforcing agents, antioxidants, colorants, pigments, etc. Exemplary of these are carbon black, glass fiber, clay, mica, graphite fiber, titanium dioxide, carbon fibers and natural fibers.

[0025] In all of the Examples herein the orifices had a circular cross section (AA and BB).

EXPERIMENTAL APPARATUS FOR EXAMPLES 1-3

[0026] A 57 mm twin-screw Werner & Pfleiderer (W&P) extruder was used to melt the polymer and develop sufficient pressure to force the resin through the die. With the exception of the test die, all operating conditions, in terms of barrel temperatures, screw rpm, feed rates, etc. used were normal processing conditions for the polymer tested.

[0027] Rynite® and Zytel® resins are commercially available from E. I. du Pont de Nemours and Company.

EXAMPLE 1

[0028] The die plate used had holes for two die inserts. The inserts were placed into the die plate from the rear and secured with a retainer ring. The first insert, which was the control, had a standard configuration with a 4.5 mm diameter die land and an aspect ratio of 3/1. The second insert, the test orifice, had a flared section at the end of the die, as shown in Figure 2. The inner diameter in the first section of the die land (shown as 1 in Figure 2) was 4.5 mm, as with the control die. The inner diameter of the flared section (indicated by 2 in Figure 2) was 5.4 mm, giving a diameter ratio of 1.2. The ratio of the area in the expanded section to the unexpanded section was 1.44. The depth of the flare from the face into the die (shown as 3 in Figure 2) was 6 mm, or 1.33 times the original diameter.

[0029] The total throughput of resin was 68 kg/hr, or 34 kg/hr/orifice. The resin tested was Zytel® 70G33, nylon 6,6 reinforced with 33% chopped glass fiber. Within 30 seconds after startup, accumulation of drips was evident at the exit of the strand from the standard die. The strand exiting from the flared die showed improved strand quality and no drips. Five minutes after startup, the exit face of the die surrounding the flared die was still clean. The exit face surrounding the standard die was surrounded with die drips which were approximately 1/8-1/4" long and beginning to turn brown due to thermal degradation.

EXAMPLE 2

[0030] The extruder and die plate were identical to those described in Example 1. The resin tested was Rynite® 530, a blend containing primarily of poly(ethylene terephthalate) resin and 30% chopped glass fiber. The test was run with a throughput of 68 kg/hr through 2 orifices. An extremely rapid buildup of drips was observed on the standard die, with significant accumulation in less than 2 minutes. Small droplets of molten resin were observed surrounding the flared die exit shortly after startup. After 5 minutes, the die face surrounding the standard die was coated with a mixture of resin and fiberglass, and substantial degradation was evident. The die face surrounding the flared die showed the original droplets but no growth had occurred. After

10 minutes, large accumulations of drips were evident at the standard die, and the drips were beginning to interfere with the flow of the strand. The flared die still showed no growth of the initial droplets.

EXAMPLE 3

[0031] The extruder and die plate were identical to those described above. The resin tested was Zytel® 103, an unreinforced nylon-6,6 resin. Approximately 20 minutes after startup, the standard die showed growth of drips surrounding the exit of the strand from the die. The die face surrounding the flared die remained clear. Sixty minutes after startup, growth of the accumulations around the standard die had continued and the flared die remained clear. Although the rate of accumulation of die drips on the standard straight through die was slower for unreinforced resins than for the two reinforced resins cited in Examples 1 and 2, the flared die provided an operating improvement vs. the standard straight through die.

EXAMPLE 4

[0032] A 40 mm W&P twin-screw extruder was used to melt the resin and develop pressure sufficient to force the melt through the die plate. The die plate used was the same as described in Example 1 above. The resin tested was Rynite® 530 at 68 kg/hr. The diameter of the original land (1 in Figure 2) was 4.5 mm. The diameter of the flared section (2 in Figure 2) was 5.4 mm. The flared section extended 6.0 mm back from the face of the die. The second orifice tested had two expansions, from 4.5 mm to 4.8 mm and from 4.8 mm to 5.4 mm (diameter ratios of 1.067 and 1.125). Each flared section had a length of 4 mm. Both of these configurations were effective in reducing the accumulation of die drips at the die face exit when compared to the standard, straight-through die design.

EXAMPLE 5

[0033] A 40 mm W&P twin-screw extruder was used to melt the resin and develop pressure sufficient to force the melt through the die plate. The die plate used was the same as described above. The resin tested was Rynite® 530 at 68 kg/hr. The extruder was operated at normal processing conditions. The first orifice tested was the flared orifice with 1.2x ratio of diameters described above in Example 4. The second die tested had three expansions, from 4.5 mm to 4.8 mm, from 4.8 mm to 5.05 mm and from 5.05 to 5.4 mm. Each flared section had a length of 3 mm. Both of these configurations were effective in reducing the accumulation of die drips at the die face exit when compared to the standard, straight-through die design.

Claims

1. A die having flared orifices for the extrusion of polymers, comprising, a die body having one or more flared orifices having the following components: 5
 - a first zone having surface S_1 ;
 - a second zone having surface S_2 ;
 - a third zone having surface S_3 ;
 - a length L_1 which is the total length of said first, 10 second and third zones;
 - a length L_3 which is the length of said third zone; and
 - a polymer flow axis A;
 - said die having a surface S_5 on a discharge 15 side of said die,
 - A and S_3 being perpendicular to S_5 ;
 - the shape of said first zone and the shape of said third zone being geometrically similar;
 - if said second zone has a one step area 20 change, the angle T formed by S_2 and A being about 45° to about 90° ;
 - if said second zone has more than one step area change, the analogous angle of each step corresponding to said angle T being 45° to 90° ; 25 and
 - the area of the orifice in said third zone being about 1.1 to about 1.7 times the area of the orifice at said first zone;
 - characterized in that: 30
 - L_1/L_3 is about 2 or more;
 - L_3 is long enough so that a polymer going through said orifice is in substantial contact with the periphery of S_3 before exiting said orifice but not substantially longer. 35
2. The die as recited in claim 1 wherein L_1/L_3 is about 3 to about 10.
3. The die as recited in claim 1 wherein S_1 is approxi- 40 mately parallel to A.
4. The die as recited in claim 1 wherein the angle T or analogous angles are about 60° to about 90° . 45
5. The die as recited in claim 1 wherein the area of the orifice in said third zone is about 1.30 to about 1.45 times the area of the orifice in said first zone.
6. The die as recited in claim 1 wherein L_1/L_3 is about 50 3 to about 10, S_1 is approximately parallel to A, the angle T or analogous angles are about 60° to about 90° , and the area of the orifice in said first zone is about 1.30 to about 1.45 times the area of the orifice in said third zone. 55
7. A polymer extrusion apparatus comprising a die according to any one of claims 1 to 6 and a means

for pumping a polymer through that die.

8. Use of a die according to any one of claims 1 to 6 for the extrusion of polymer through the die.

Patentansprüche

1. Düse mit aufgeweiteten Öffnungen für die Extrusion von Polymeren, umfassend einen Düsenkörper mit einer oder mehreren aufgeweiteten Öffnungen mit den folgenden Teilen:
 - eine erste Zone mit Oberfläche S_1 ;
 - eine zweite Zone mit Oberfläche S_2 ;
 - eine dritte Zone mit Oberfläche S_3 ;
 - eine Länge L_1 , die die Gesamtlänge der ersten, zweiten und dritten Zone ist;
 - eine Länge L_3 , die die Länge der dritten Zone ist; und
 - eine Polymerströmungsachse A;
 - wobei die Düse auf einer Austrittsseite der Düse eine Oberfläche S_5 aufweist,
 - A und S_3 senkrecht zu S_5 sind;
 - die Form der ersten Zone und die Form der dritten Zone geometrisch ähnlich sind;
 - wenn die zweite Zone eine einstufige Flächenänderung aufweist, der durch S_2 und A gebildete Winkel T etwa 45° bis etwa 90° beträgt;
 - wenn die Zweite Zone mehr als eine einstufige Flächenänderung aufweist, der dem Winkel T entsprechende analoge Winkel jeder Stufe 45° bis 90° beträgt; und
 - die Fläche der Öffnung in der dritten Zone etwa 1,1 bis etwa 1,7 mal die Fläche der Öffnung an der ersten Zone ist;
 - dadurch gekennzeichnet, daß:
 - L_1/L_3 etwa 2 oder mehr beträgt;
 - L_3 lang genug ist, so daß ein durch die Öffnung hindurchtretendes Polymer in wesentlichem Kontakt mit dem Umfang von S_3 ist, bevor es die Öffnung verläßt, aber nicht wesentlich länger.
2. Düse nach Anspruch 1, bei der L_1/L_3 etwa 3 bis etwa 10 beträgt.
3. Düse nach Anspruch 1, bei der S_1 ungefähr parallel zu A ist.
4. Düse nach Anspruch 1, bei der der Winkel T oder analoge Winkel etwa 60° bis etwa 90° betragen.
5. Düse nach Anspruch 1, bei der die Fläche der Öffnung in der dritten Zone etwa 1,30 bis etwa 1,45 mal die Fläche der Öffnung in der ersten Zone ist.
6. Düse nach Anspruch 1, bei der L_1/L_3 etwa 3 bis etwa 10 beträgt, S_1 ungefähr parallel zu A ist, der

Winkel T oder analoge Winkel etwa 60° bis etwa 90° betragen und die Fläche der Öffnung in der ersten Zone etwa 1,30 bis etwa 1,45 mal die Fläche der Öffnung in der dritten Zone ist.

7. Polymer-Extrusionsvorrichtung, umfassend eine Düse nach einem der Ansprüche 1 bis 6 und eine Einrichtung zum Pumpen eines Polymers durch diese Düse.

8. Verwendung einer Düse nach einem der Ansprüche 1 bis 6 zur Extrusion eines Polymers durch die Düse.

Revendications

1. Filière présentant des orifices évasés pour l'extrusion de polymères, comprenant un corps de filière avec un ou plusieurs orifices évasés possédant les composants suivants:

une première zone avec une surface S_1 :
 une deuxième zone avec une surface S_2 :
 une troisième zone avec une surface S_3 :
 une longueur L_1 qui représente la longueur totale desdites première, deuxième et troisième zones:
 une longueur L_3 qui représente la longueur de ladite troisième zone: et
 un axe d'écoulement de polymère A:
 ladite filière présentant une surface S_5 sur le côté décharge de ladite filière,
 A et S_3 étant perpendiculaires à S_5 :
 la forme de ladite première zone et la forme de ladite troisième zone étant similaires du point de vue géométrique:
 si ladite deuxième zone présente un changement de surface en une étape, l'angle T formé par S_2 et A étant d'environ 45° à environ 90°:
 si ladite deuxième zone présente un changement de surface en plus d'une étape, l'angle analogue de chaque étape correspondant audit angle T étant de 45° à 90°; et
 la surface de l'orifice dans ladite troisième zone étant d'environ 1,1 à environ 1,7 fois la surface de l'orifice au niveau de ladite première zone: caractérisée en ce que:
 L_1/L_3 est supérieur ou égal à environ 2;
 L_3 est une longueur suffisante pour qu'un polymère passant à travers ledit orifice se trouve en contact substantiel avec la périphérie de S_3 avant de sortir dudit orifice mais n'est pas substantiellement plus longue.

2. Filière suivant la revendication 1, dans laquelle L_1/L_3 est d'environ 3 à environ 10.

3. Filière suivant la revendication 1, dans laquelle S_1

est approximativement parallèle à A.

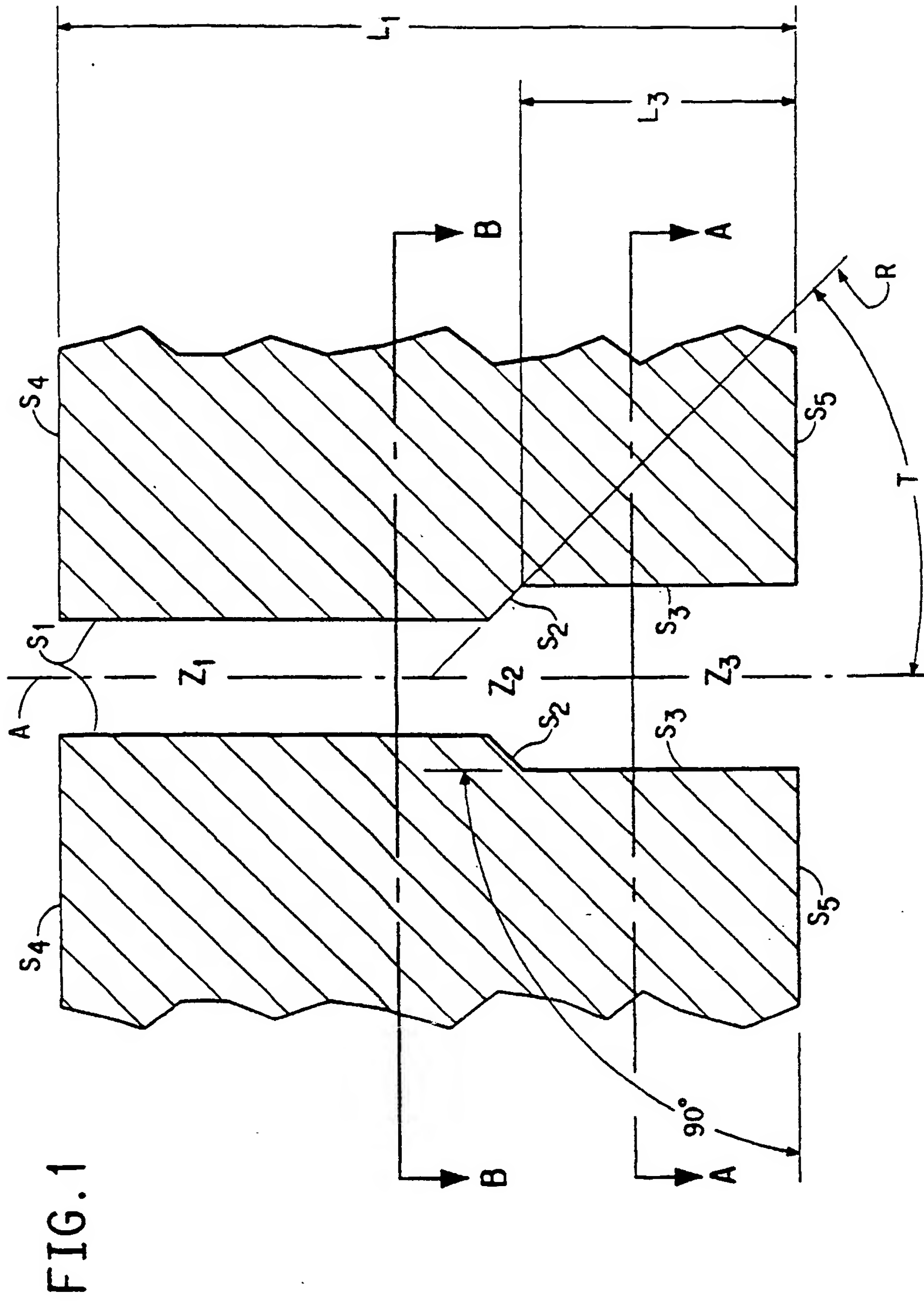
4. Filière suivant la revendication 1, dans laquelle l'angle T ou les angles analogues sont d'environ 60° à environ 90°.

5. Filière suivant la revendication 1, dans laquelle la surface de l'orifice dans ladite troisième zone est d'environ 1,30 à environ 1,45 fois la surface de l'orifice dans ladite première zone.

6. Filière suivant la revendication 1, dans laquelle L_1/L_3 est d'environ 3 à environ 10, S_1 est approximativement parallèle à A, l'angle T ou les angles analogues sont d'environ 60° à environ 90° et la surface de l'orifice dans ladite première zone est d'environ 1,30 à environ 1,45 fois la surface de l'orifice dans ladite troisième zone.

7. Appareil d'extrusion de polymères comprenant une filière suivant l'une quelconque des revendications 1 à 6 et un dispositif de pompage d'un polymère à travers cette filière.

8. Utilisation d'une filière suivant l'une quelconque des revendications 1 à 6 pour l'extrusion de polymère à travers la filière.



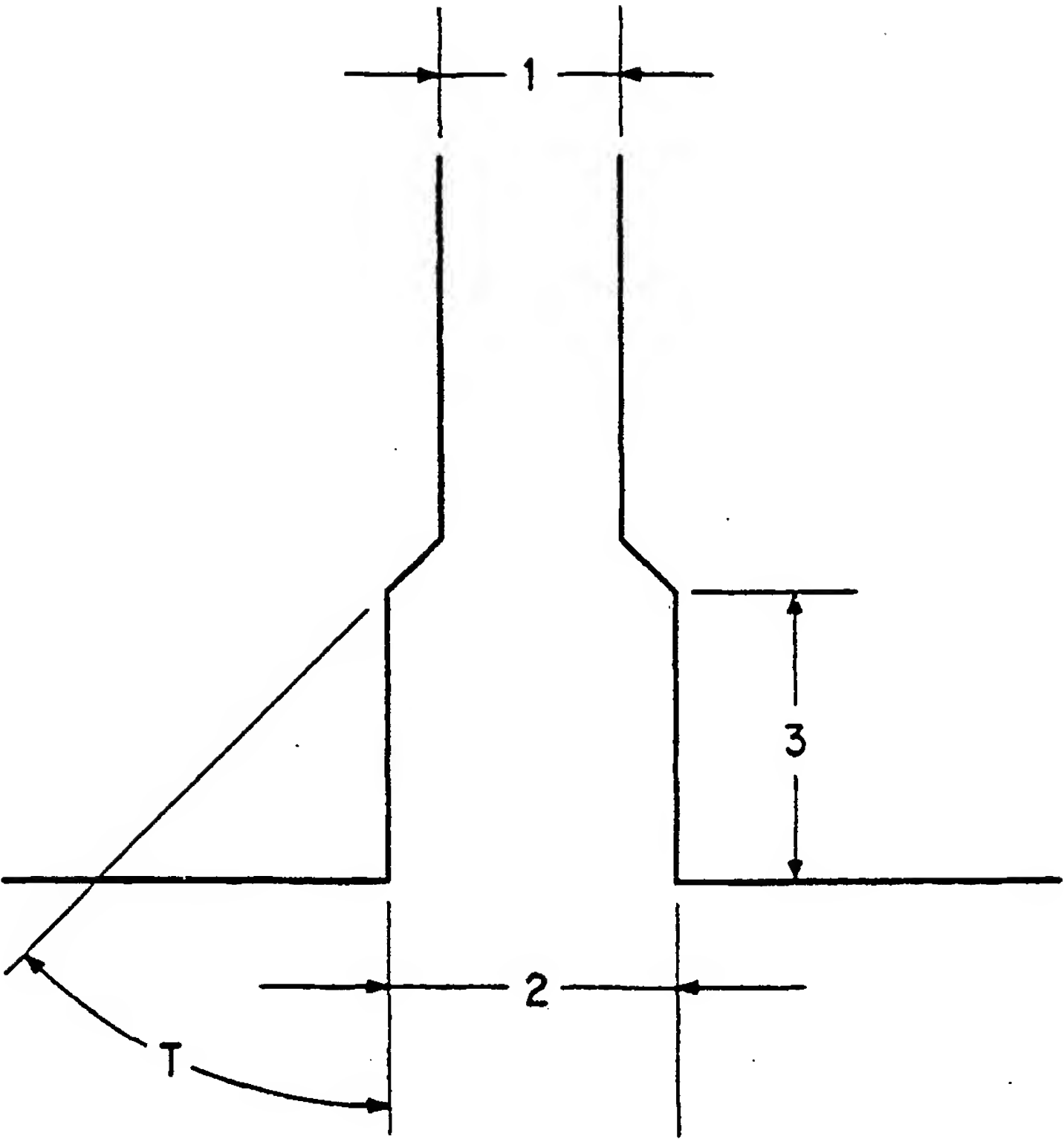


FIG.2